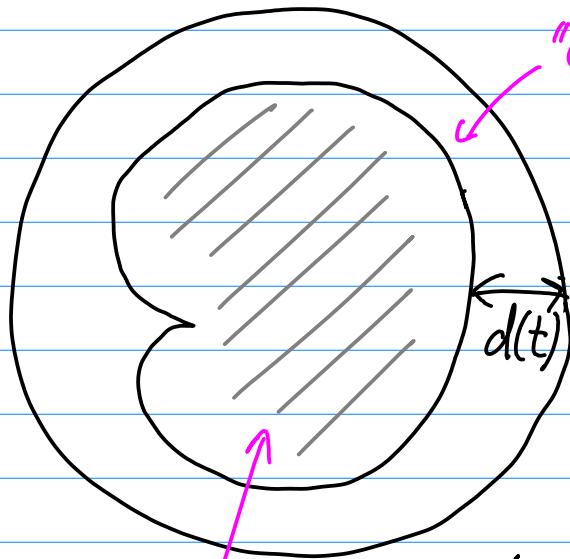


# Mixing hits a wall

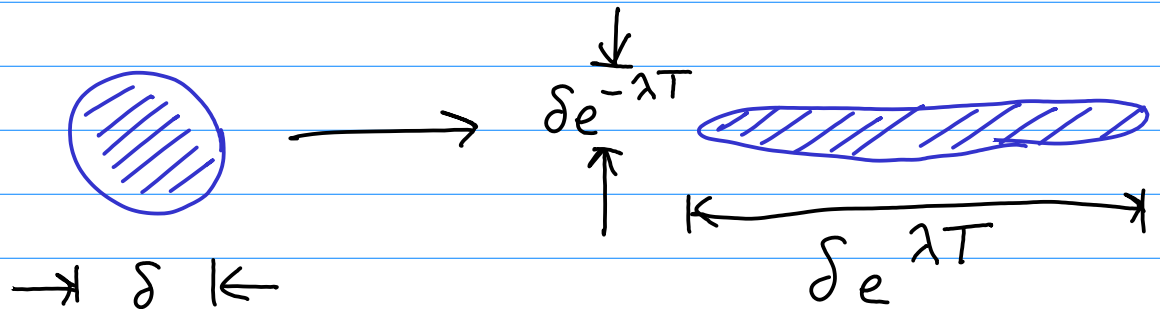
GFD, 6/30/2008



The mixing pattern is caused by some periodic stirring mechanism.

At every period  $T$ , some white fluid is shaved from the edge, decreasing the distance  $d(t)$ .

What happens inside the mixing region? Assume a very simple **chaotic mixer**, meaning that fluid elements are stretched at rate  $\lambda$ : (on average)



The maximum width a dye filament can have is given by the Batchelor length,

$$l = \sqrt{\frac{\kappa}{\lambda}}$$

$\kappa$  = molecular diffusivity

(Balance between diffusion and strain)

The width of a white filament injected at time  $t$  is

$$\Delta(t) = d(t) - d(t+T) \simeq -T \dot{d}(t)$$

since  $d$  changes little at each period.

Now, if a white filament is injected at time  $\tau < t$ , how long does it last? "age" of filament

$$\underbrace{\Delta(\tau)}_{\text{initial width}} \underbrace{e^{-\lambda(t-\tau)}}_{\text{compression } t > \tau} = \underbrace{l}_{\text{Batchelor length}}$$

In other words, solving for  $\tau(t)$  in the above gives us the injection time of the oldest filaments still visible at time  $t$ . Filaments injected before  $\tau(t)$  are below the Batchelor length, so they are no longer white.

At some point the injected filament width will equal the Batchelor length:

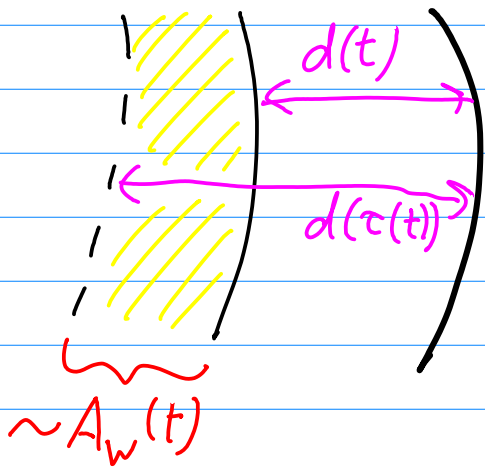
$$\Delta(t_B) = l$$

so that  $\tau(t_B) = t_B$ .

It makes no sense to speak of those filaments as "white", since they are dominated by diffusion. Hence, assume  $t < t_B$ .

Now, in the experiments we measure the number of "white pixels" in the central mixing region. This is proportional to the area of white material injected,

$$A_w(t) \sim d(\tau(t)) - d(t)$$



We've gone as far as we can without introducing some form for  $d(t)$ .

First assume  $d(t) = d_0 e^{-\mu t}$

$$\Delta(t) = -T \dot{d} = d_0 \mu T e^{-\mu t} = \Delta_0 e^{-\mu t}$$

$$\Delta(t_B) = l \Rightarrow t_B = \frac{1}{\mu} \log \left( \frac{d_0 \mu T}{l} \right)$$

Solve for  $\tau(t)$ : ( $d_0 \mu T > l$ )

$$\Delta_0 e^{-\mu \tau} e^{-\lambda(t-\tau)} = l$$

$$e^{(\lambda-\mu)\tau} = \left( \frac{l}{\Delta_0} \right) e^{\lambda t}$$

$$\tau = \frac{1}{\lambda-\mu} \left[ \log \left( \frac{l}{\Delta_0} \right) + \lambda t \right]$$

$$= \frac{1}{\lambda-\mu} \left( -\mu t_B + \lambda t \right)$$

$$\tau(t) = \frac{\lambda t - \mu t_B}{\lambda - \mu}$$

$$\tau - t = \frac{\cancel{\lambda t} - \mu t_B - (\cancel{\lambda - \mu})t}{\lambda - \mu} = \frac{\mu(t - t_B)}{\lambda - \mu}$$

Now, by assumption:  $\tau < t < t_B$ :

$$\underbrace{t - \tau}_{> 0} = \frac{\mu}{\lambda - \mu} \underbrace{(t_B - t)}_{> 0}$$

Hence, for consistency we require  $\mu < \lambda$ .

i.e., the rate of approach to the wall is slower than the rate of stretching in the mixing region. Otherwise the wall has no effect: the wall region is depleted faster than filaments can reach the Batchelor scale.

If  $\mu < \lambda$ , we have

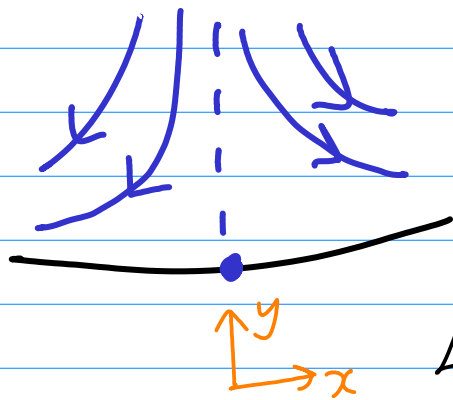
$$\begin{aligned} A_w(t) &\sim d(\tau(t)) - d(t) \\ &\sim d_0 (e^{-\mu\tau} - e^{-\mu t}) \\ &\sim d_0 e^{-\mu t} (e^{(t-\tau)\mu} - 1) \\ &\sim d_0 e^{-\mu t} \left( \exp\left(\frac{\mu^2}{\lambda - \mu} (t_B - t)\right) - 1 \right) \end{aligned}$$

We see that for  $t \ll t_B$ ,  $A_w(t) \sim e^{-\mu t}$ .

So the decay rate of the "white" area is completely dominated by the walls. The central mixing process is efficient ( $\lambda > \mu$ ), but it is "starved" by the boundary.

So what happens in practice?

The "figure-8" protocol shown has a reattachment point:



Let's model it as a steady flow (we can take the time-dependence into account by using a map rather than a flow).

Let  $x$  be the "along wall" coordinate.

Taylor in  $y$ :

$$u(x, y) = u_0(x) + u_1(x)y + \dots$$

no slip

$$v(x, y) = v_0(x) + v_1(x)y + v_2(x)y^2 + \dots$$

no throughflow

$$\text{Now, } \nabla \cdot \underline{u} = 0 \Rightarrow u_1'(x)y + v_1(x) + v_2(x)2y = 0$$

Equating terms, we find  $u_1(x) = 0$ ,  $u_2(x) = -\frac{1}{2} u_1'(x)$ .

Letting  $u_1(x) = A(x)$ , get

$$u(x, y) = A(x)y + O(y^2)$$

$$v(x, y) = -\frac{1}{2} A'(x)y^2 + O(y^3)$$

This is a "boundary layer" form.

A reattachment point corresponds to  $A(x)$  changing sign, say at  $x=0$ , with  $A'(0) > 0$ .

Hence, along the separatrix we can solve for the motion of a fluid particle,

$$\dot{y} = v(0, y) = -\frac{1}{2} A'(0)y^2$$

This has solution

$$y(t) = \frac{y_0}{1 + A'(0)t y_0} \sim \frac{1}{A'(0)t}, \quad t \text{ large.}$$

Note that asymptotically a particle "forgets" its initial condition  $y_0$ . This explains why material lines "bunch up" against each other faster than they approach the wall.



There is a visible "front".

Now we have our asymptotic form for  $d(t)$ :

$$d(t) \sim \frac{1}{A'(0)t}, \quad t \gg 1.$$

$$\text{Hence, } \Delta(t) = -T d(t) \sim \frac{T}{A'(0)t^2}.$$

We have  $A_w(t) = d(\tau(t)) - d(t)$

$$\text{with } \Delta(\tau) e^{-\lambda(t-\tau)} = l.$$

$$A_w = \frac{1}{A'(0)\tau} - \frac{1}{A'(0)t} = \frac{1}{A'(0)} \frac{(t-\tau)}{\tau t}$$

$$\text{But also, } \log \Delta - \lambda(t-\tau) = \log l$$

$$\text{or } t - \tau = \frac{1}{\lambda} \log(\Delta(\tau)/l)$$

$\Delta(\tau)$  is algebraic, so for large time the RHS is not large. Hence, for large time we must have

$$t/\tau \simeq 1, \quad t \gg 1,$$

We conclude:

$$A_w \sim \frac{1}{A'(0)} \frac{\log(T/A'(0)l t^2)}{\lambda t^2}$$

$$t \gg 1 \quad (\text{but } t < t_B)$$

This power-law decay is consistent with the data.

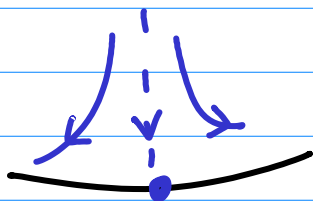
In a simple "parabolic baker's map" model, reproduces data extremely well for long times.

In experiments, determining  $\lambda$  is the most difficult part.

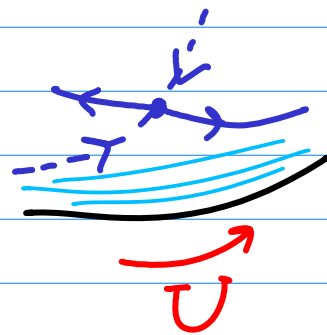
To improve the mixing rate, spin the wall!

$$u(x,y) = U + A(x)y + O(y^2)$$
$$v(x,y) = -\frac{1}{2}A'(x)y^2 + O(y^3)$$

The moving wall destroys the reattachment point and replaces it with a hyperbolic fixed point



Fixed wall:  
algebraic mixing



Moving wall: exponential

The price to pay is that there is now an unmixed layer near the wall.

[There are other means of destroying the reattachment points.]